

Chapter 1

1. Name one separation process that requires energy input to the system.

Ans: Distillation

2. Name one separation process that requires a matter as input to the system.

Ans: Coagulation

3. Define separation factor.

$$\text{Ans: } \alpha_{ij} = \frac{(x_{i1}/x_{j1})}{(x_{i2}/x_{j2})}$$

i,j are two components and 1,2 are two streams.

4. What is the driving force of mass transfer?

Ans: Gradient of chemical potential.

5. For no separation, what is the value of separation factor?

$$\text{Ans: } \alpha_{ij} = 1$$

Chapter 2

1. Name two equilibrium governing separation processes.

Ans: Distillation, absorption.

2. Name two rate governed separation processes.

Ans: Reverse osmosis, ultrafiltration.

3. What is the difference between absorption and adsorption?

Ans: Absorption is a bulk phenomena and adsorption is a surface phenomena.

4. What is the difference between osmosis and reverse osmosis?

Ans: In osmosis, water moves from solvent to salt side. In reverse osmosis, water is

forced out of solute side by applying pressure.

5. What is driving force of dialysis?

Ans: Concentration gradient.

Chapter 3

1. What is the difference between symmetric and asymmetric membrane?

Ans: In symmetric membrane, the material is same with uniform porosity. In asymmetric membrane, a thin skin of lower porosity over a symmetric support acts as a membrane.

2. What is the relationship of osmotic pressure with concentration and molecular weights?

Ans: Osmotic pressure decreases with molecular weight and increases with concentration.

3. What is the relationship between observed and real retention?

Ans: Real retention > observed retention.

4. Consider filtration of 5 kg/m³ concentration of ultrafiltration is gel layer controlled

with gel concentration of 150 kg/m³. Filtration occurs in a tube of diameter 25 mm and length 1m. The flow rate is 150 L/h, protein diffusivity is 3x10⁻¹¹ m²/s. Find the permeate flux?

$$\begin{aligned} \text{Ans: } J = \text{Permeate flux} &= k \ln \frac{c_g}{c_0} \\ &= k \ln \frac{150}{5} = 3.4k \end{aligned}$$

Estimation of k:

$$\text{For tubes, } Sh = \frac{kd}{D} = 1.62 \left(\text{Re} Sc \frac{d}{L} \right)^{\frac{1}{3}}$$

$$k = 1.62 \left(\frac{D^3}{d^3} \cdot \frac{u_0 d}{r} \cdot \frac{r d}{D L} \right)^{\frac{1}{3}}$$

$$= 1.62 \left(\frac{u_0 D^2}{dL} \right)^{\frac{1}{3}}$$

$$Q = 150 \text{ L/h} = \frac{150 \times 10^{-3}}{3600} \text{ m}^3/\text{s} = 4.17 \times 10^{-5} \text{ m}^3/\text{s}$$

$$u_0 = \frac{Q}{A} = \frac{4.17 \times 10^{-5}}{\pi (25 \times 10^{-3})^2 / 4} = 0.085 \text{ m/s}$$

$$k = 1.62 \left(\frac{0.085 \times 9 \times 10^{-22}}{25 \times 10^{-3} \times 1} \right)^{\frac{1}{3}} = 2.35 \times 10^{-7} \text{ m/s}$$

$$J = 2.35 \times 10^{-7} \times 3.4 = 8 \times 10^{-7} \text{ m}^3/\text{m}^2 \cdot \text{s}$$

5. Consider reverse osmosis of salt solution at a concentration of 10 kg/m^3 , in a thin

channel of length 2 m and equivalent diameter of 2 mm. The membrane permeability is $2 \times 10^{-12} \text{ m}^3/(\text{N} \cdot \text{s})$. The real retention is 0.95. $\Delta P = 2500 \text{ kPa}$ and $u_0 = 1.0 \text{ m/s}$. The osmotic pressure of salt is $\pi(\text{pa}) = 85000c$ (c is in kg/m^3) and salt diffusivity is $1.5 \times 10^{-9} \text{ m}^2/\text{s}$. Find the permeate flux and concentration assuming a film theory?

$$\text{Ans: } C_0 = 10 \text{ kg/m}^3; \quad L_p = 2 \times 10^{-12} \text{ m}^3/\text{N} \cdot \text{s}; \quad L = 2 \text{ m}; \quad d_e = 2 \text{ mm}; \quad R_r = 0.95;$$

$$\Pi = 85000C; \quad D = 1.5 \times 10^{-9} \text{ m}^2/\text{s}; \quad u_0 = 1 \text{ m/s}$$

Mass transfer coefficient:

$$Sh = \frac{kd_e}{D} = 1.85 \left(Re Sc \frac{d_e}{L} \right)^{\frac{1}{3}}$$

$$Re = \frac{\rho u_0 d_e}{\mu} = 10^6 \times 1 \times 2 \times 10^{-3} = 2000$$

So laminar flow

$$k = 1.85 \left(\frac{u_0 D^2}{d_e L} \right)^{\frac{1}{3}}$$

$$= 1.85 \left(\frac{1 \times 1.25 \times 10^{-18}}{2 \times 10^{-3} \times 2} \right)^{\frac{1}{3}}$$

$$= 1.53 \times 10^{-5} \text{ m / s}$$

Film Theory:

$$j = k \ln \left(\frac{c_m - c_p}{c_0 - c_p} \right)$$

$$C_P = C_0 (1 - R_r) = 0.05 \times 10 = 0.5 \text{ kg / m}^3$$

$$J = .53 \times 10^{-5} \ln \left(\frac{C_m - 0.5}{9.5} \right)$$

Osmotic Pressure Model

$$J = L_P (\Delta P - \Delta \pi) = L_P (\Delta P - a C_m R_r)$$

$$\therefore J = 2 \times 10^{-12} (2500 \times 10^3 - 85000 \times 0.95 c_m)$$

$$J = 2 \times 10^{-12} (2.5 \times 10^6 - 8 \times 10^4 c_m)$$

$$\therefore J = 5 \times 10^{-6} (1 - 0.032 c_m) \dots\dots\dots(2)$$

From equations (1) and (2),

$$1.53 \times 10^{-5} \ln\left(\frac{c_m - 0.5}{9.5}\right) = 5 \times 10^{-6} (1 - 0.032 c_m)$$

$$3 \ln\left(\frac{c_m - 0.5}{9.5}\right) = (1 - 0.032 c_m)$$

Cm	12	15	12.5	12.2
LHS	0.573	1.26	0.7	0.62
RHS	0.616	0.52	0.6	0.61

$$\therefore C_m = 12.2 \text{ kg/m}^3$$

$$C_p = 0.05 \times 12.2 = 0.61 \text{ kg/m}^3$$

$$J = 3.05 \times 10^{-6} \text{ m}^3/\text{m}^2 \cdot \text{s}$$