



Jet Aircraft Propulsion

Prof. Bhaskar Roy, Prof. A M Pradeep

Department of Aerospace Engineering,
IIT Bombay

Lect-18

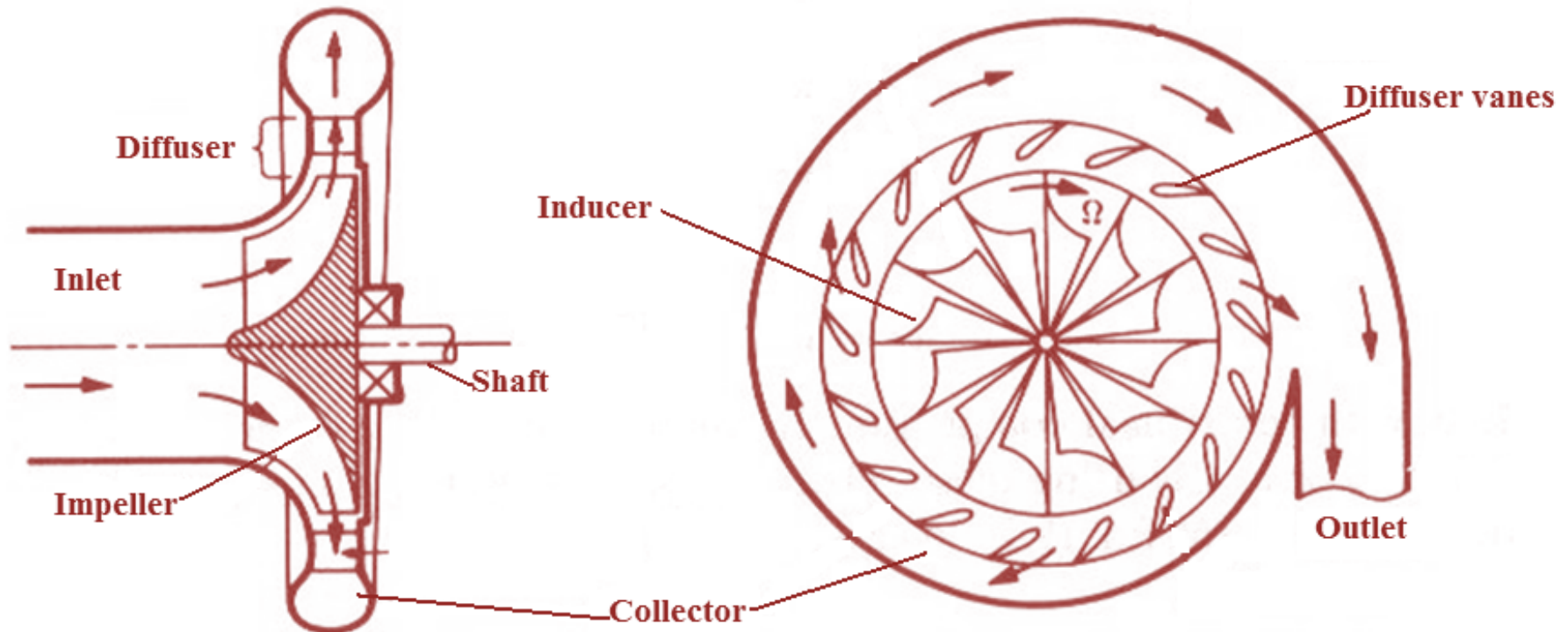
In this lecture...

- Elements of centrifugal compressors

Centrifugal compressors

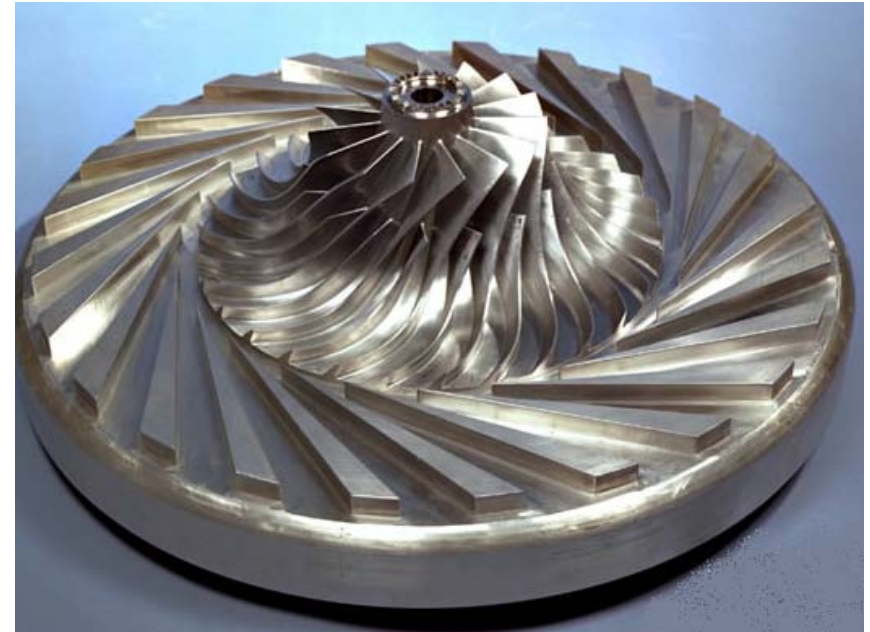
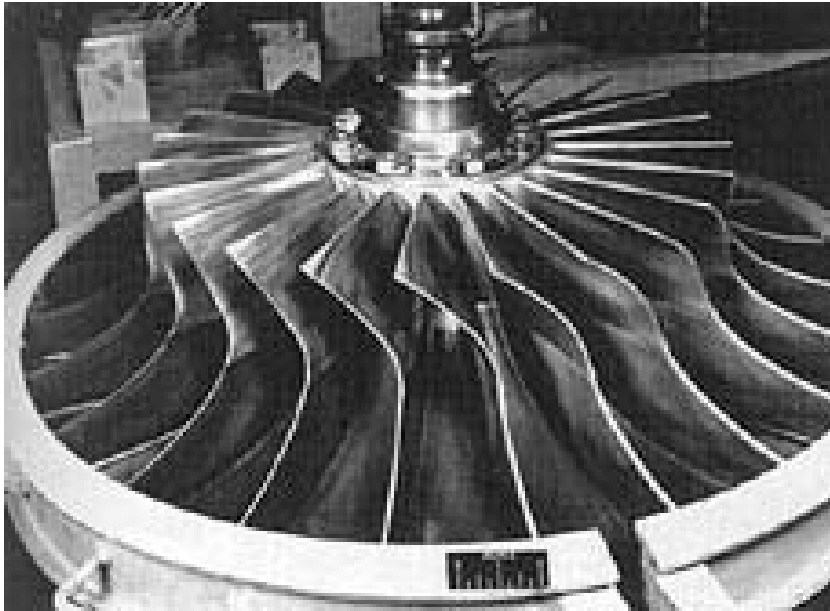
- Centrifugal compressors were used in the first jet engines developed independently by Frank Whittle and Hans Ohain.
- Centrifugal compressors still find use in smaller gas turbine engines.
- For larger engines, axial compressors need lesser frontal area and are more efficient.
- Centrifugal compressors can develop higher per stage pressure ratios.

Centrifugal compressors stage



Schematic of a typical centrifugal compressor

Centrifugal compressors stage



Typical centrifugal compressor rotors

Centrifugal compressor stage

The torque applied on the fluid by the rotor

$\tau = \dot{m}[(rC_w)_2 - (rC_w)_1]$, where 1 and 2 denotes the compressor inlet and outlet, respectively.

The total work per unit mass is therefore,

$$w = \Omega \tau / \dot{m} = \Omega [(rC_w)_2 - (rC_w)_1]$$

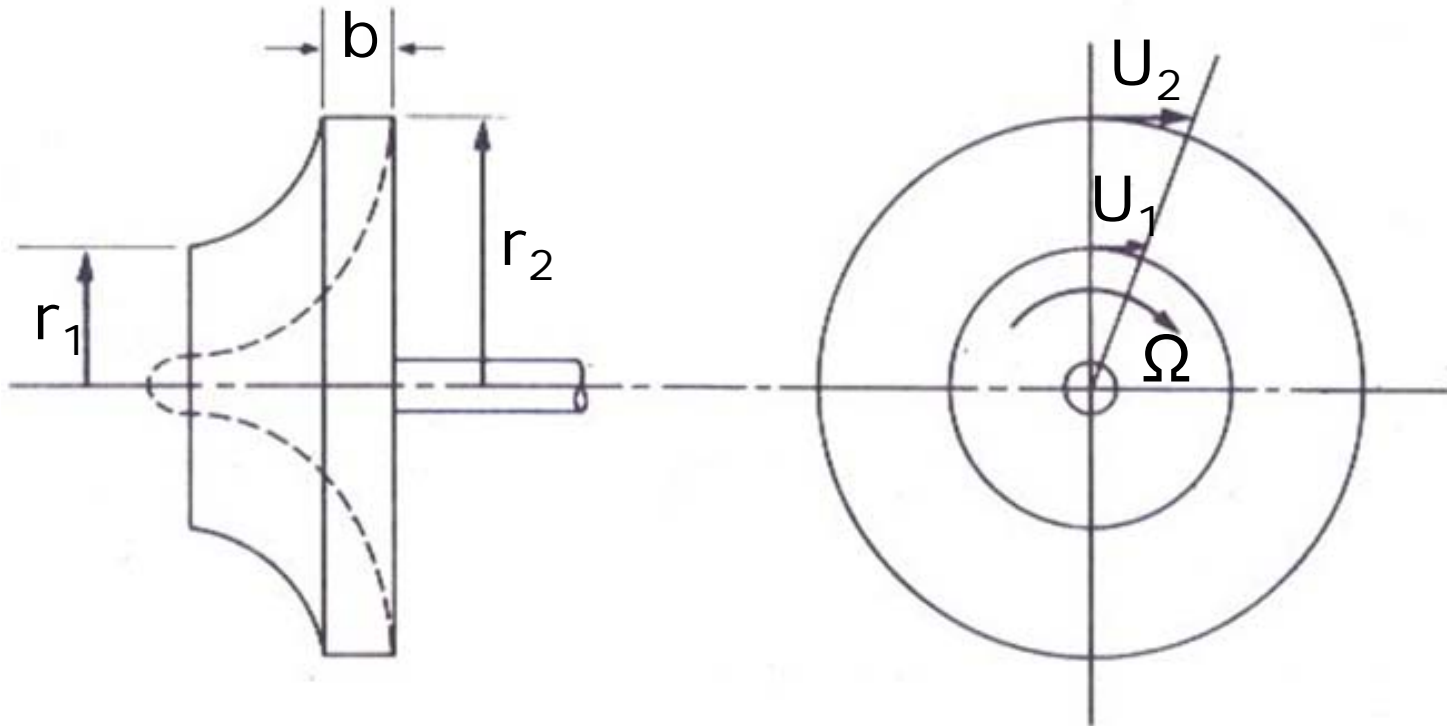
or, $w = (UC_w)_2 - (UC_w)_1$ in which, $U = \Omega r$

From the steady flow energy equation,

$$w = h_{02} - h_{01} = h_2 - h_1 + \frac{C_2^2}{2} - \frac{C_1^2}{2}$$

$$\text{or, } h_2 - h_1 = (UC_w)_2 - (UC_w)_1 - \frac{C_2^2}{2} + \frac{C_1^2}{2}$$

Centrifugal compressor stage



Centrifugal compressor stage

The above equation gets transformed to,

$$h_2 - h_1 = \frac{U_2^2}{2} - \frac{U_1^2}{2} - \left(\frac{V_2^2}{2} - \frac{V_1^2}{2} \right)$$

$$\text{i.e., } dh = d\left(\frac{\Omega^2 r^2}{2}\right) - \frac{dV^2}{2}$$

Since, $Tds = dh - dP / \rho$

$$\frac{dP}{\rho} = d\left(\frac{\Omega^2 r^2}{2}\right) - \frac{dV^2}{2} - Tds$$

$$\text{For an isentropic flow, } \frac{dP}{\rho} = d\left(\frac{\Omega^2 r^2}{2}\right) - d\left(\frac{V^2}{2}\right)$$

Centrifugal compressor stage

- For axial compressors, $dr \approx 0$ and the above equation reduces to $dP / \rho = -d(V^2 / 2)$
- Thus in an axial compressor rotor, pressure rise can be obtained only by decelerating the flow.
- In a centrifugal compressor, the term $d(\Omega^2 r^2 / 2) > 0$, means that pressure rise can be obtained even without any change in the relative velocity.
- With no change in relative velocity, these rotors are not liable to flow separation.

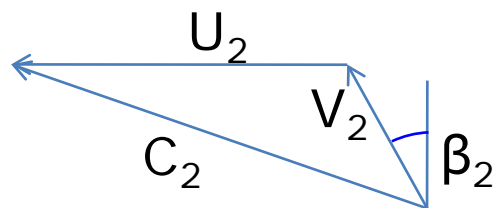
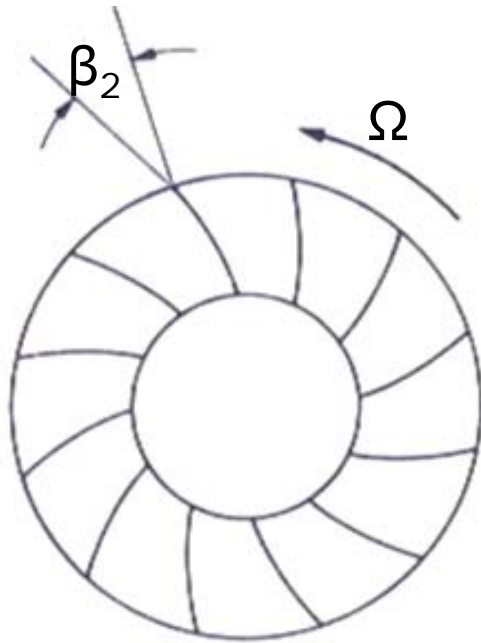
Centrifugal compressor stage

- However most centrifugal compressors do have deceleration and hence are liable to boundary layer separation,
- Centrifugal compressor rotor is not essentially limited by separation the way axial compressor is.
- It is therefore possible to obtain higher per stage pressure rise from a centrifugal compressor as compared to axial flow compressors.

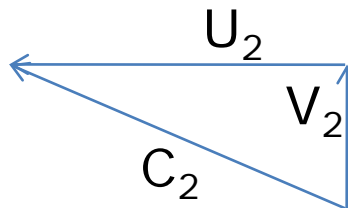
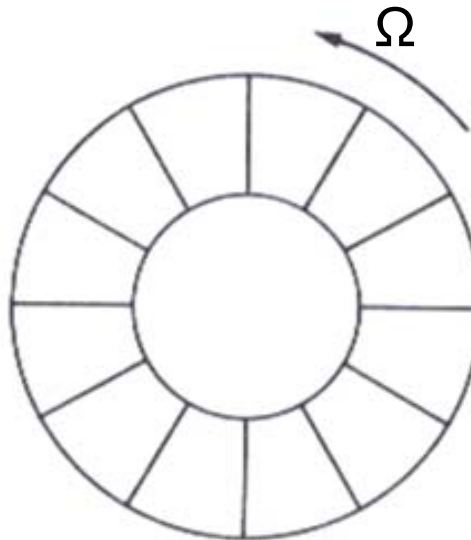
Impeller

- In principle, there are three possibilities for a centrifugal compressor rotor.
 - Straight radial
 - Forward leaning
 - Backward leaning
- Forward leaning blades are not used due inherent dynamic instability.
- Straight and backward leaning blades are commonly used in modern centrifugal compressor rotors.

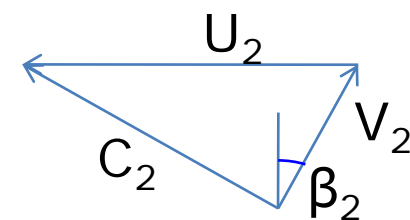
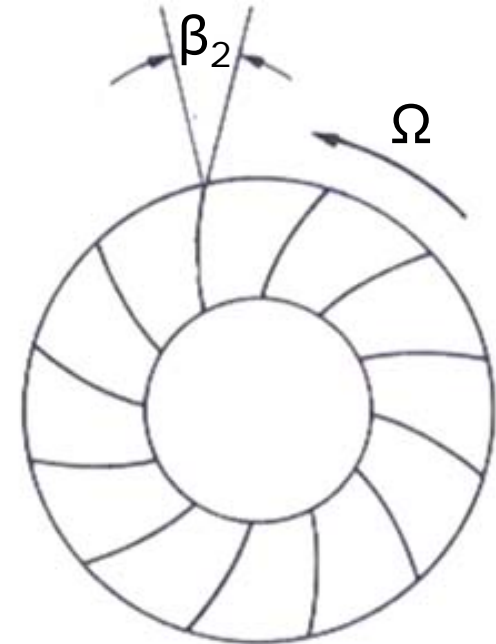
Impeller



Forward leaning blades
(β_2 is negative)



Straight radial

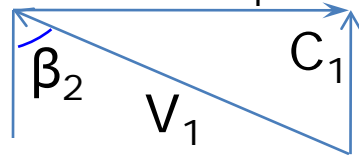
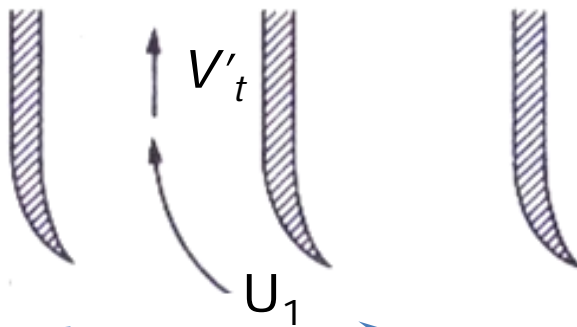
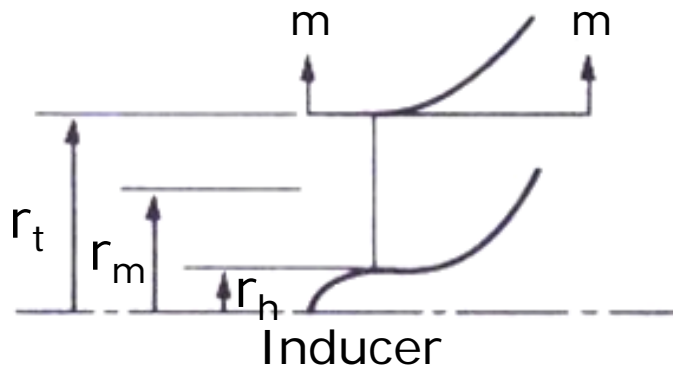


Backward leaning blades
(β_2 is positive)

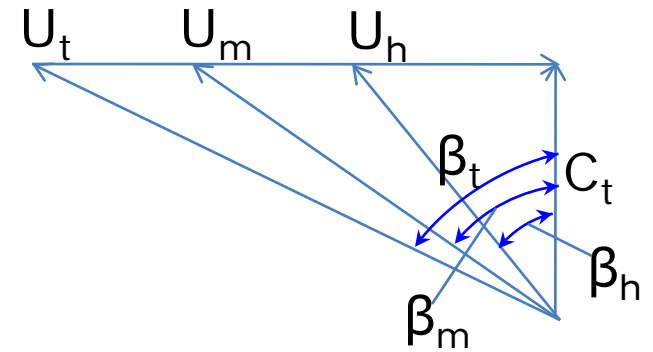
Inducer

- Inducer is the impeller entrance section where the tangential motion of the fluid is changed in the radial direction.
- This may occur with a little or no acceleration.
- Inducer ensures that the flow enters the impeller smoothly.
- Without inducers, the rotor operation would suffer from flow separation and high noise.

Inducer



Section m-m



Leading edge velocity triangles

Inducer

- It can be seen from the above that

$$V'_t = V_{1t} \cos \beta_{1t}$$

Where, V' denotes the relative velocity at the inducer outlet.

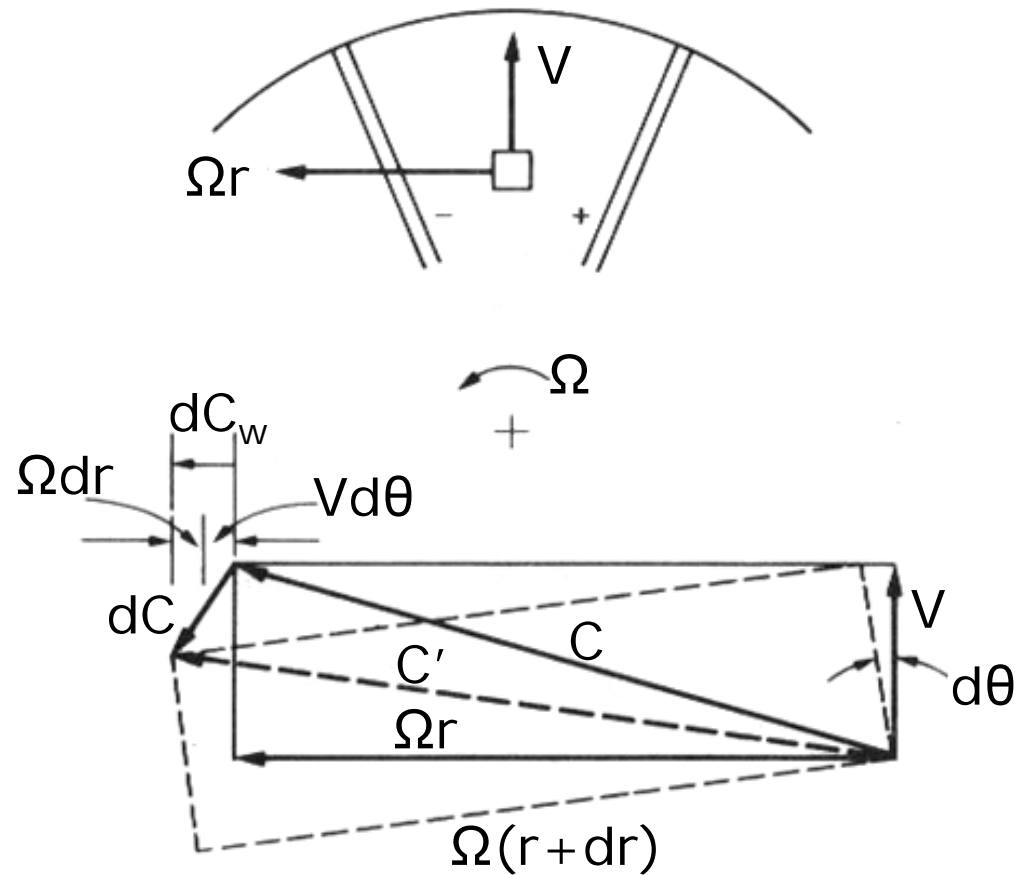
- It can be seen that $V' < V_1$, which indicates diffusion in the inducer.
- Similarly, we can see that the relative Mach number from the velocity triangle is,

$$M_{1rel} = M_1 / \cos \beta_{1t}$$

Coriolis acceleration

- We have discussed earlier that pressure change due to the centrifugal force field is not a cause of boundary layer separation.
- This can also be explained by the Coriolis forces that are present in centrifugal compressor rotors.
- Let us consider a fluid element travelling radially outward in the passage of a rotor.
- We shall examine the velocity triangles of this fluid during a time period dt .

Coriolis acceleration



Coriolis acceleration

- The magnitude of the relative velocity is unchanged, but the particle has suffered an absolute change of velocity.

$$dV_w = \Omega dr + Vd\theta$$

$$\text{or, } dV_w = \Omega Vdt + V\Omega dt,$$

Thus, the Coriolis acceleration, $a_\theta = 2\Omega V$

and it requires a pressure gradient in the tangential

direction of magnitude, $\frac{1}{r} \frac{\partial P}{\partial \theta} = -2\rho\Omega V$

Coriolis acceleration

- The existence of the tangential pressure gradient means that there will be a positive gradient of V in the tangential direction.

$$\frac{1}{\rho} \frac{dP}{rd\theta} = - \frac{d(V^2 / 2)}{rd\theta} = - \frac{V}{r} \frac{dV}{d\theta}$$

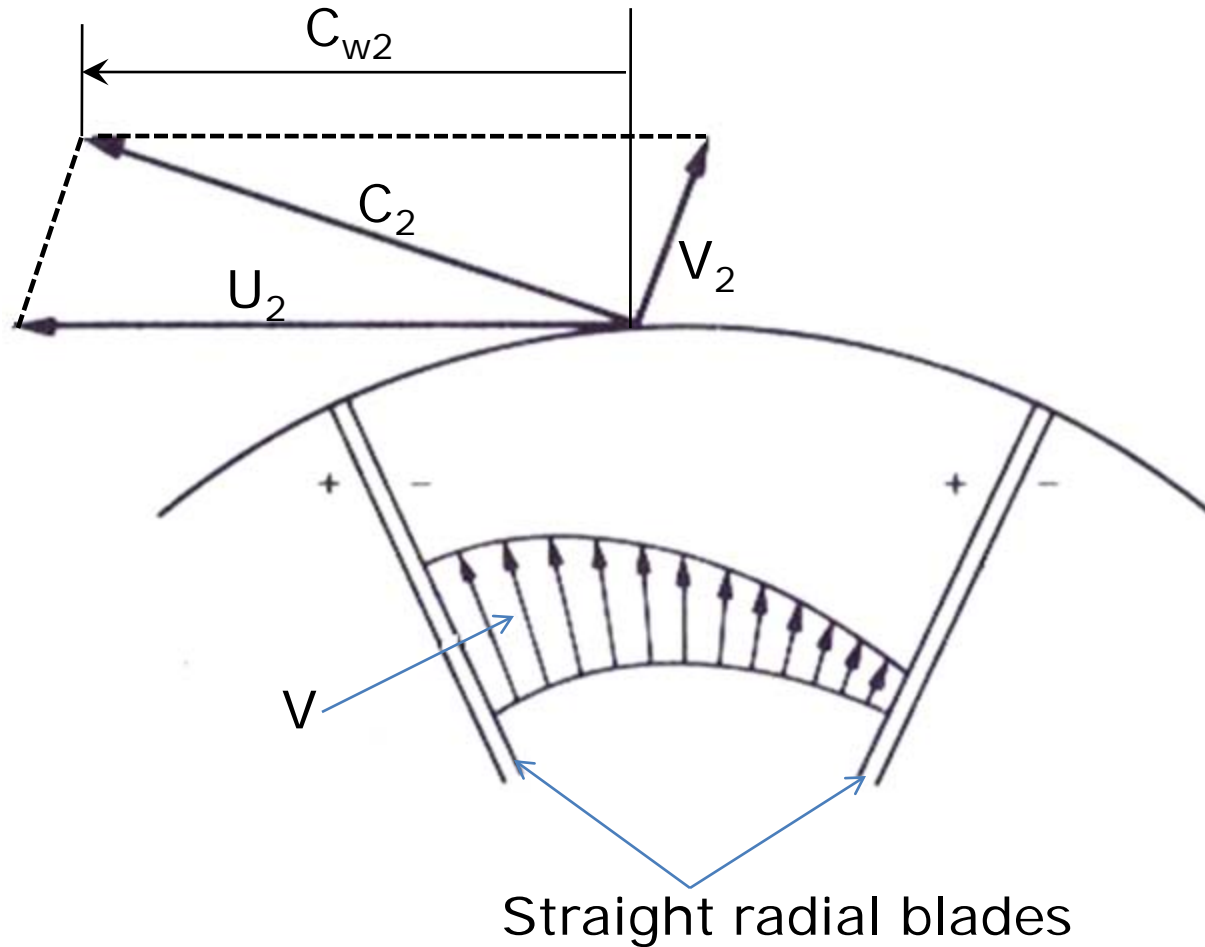
$$\text{Therefore, } \frac{1}{r} \frac{dV}{d\theta} = 2\Omega$$

- This means that there will be a tangential variation in relative velocity.

Slip factor

- Towards the outlet of the impeller, as the Coriolis pressure gradient disappears, there will be a difference between V_{w2} and U_2 .
- This difference in the velocities is expressed as **slip factor**, $\sigma_s = V_{w2} / U_2$
- The slip factor is approximately related to the number of blades of the impeller.
- For a straight radial blade, the slip factor is empirically expressed as $\sigma_s \approx 1 - 2/N$, where N is the number of blades.

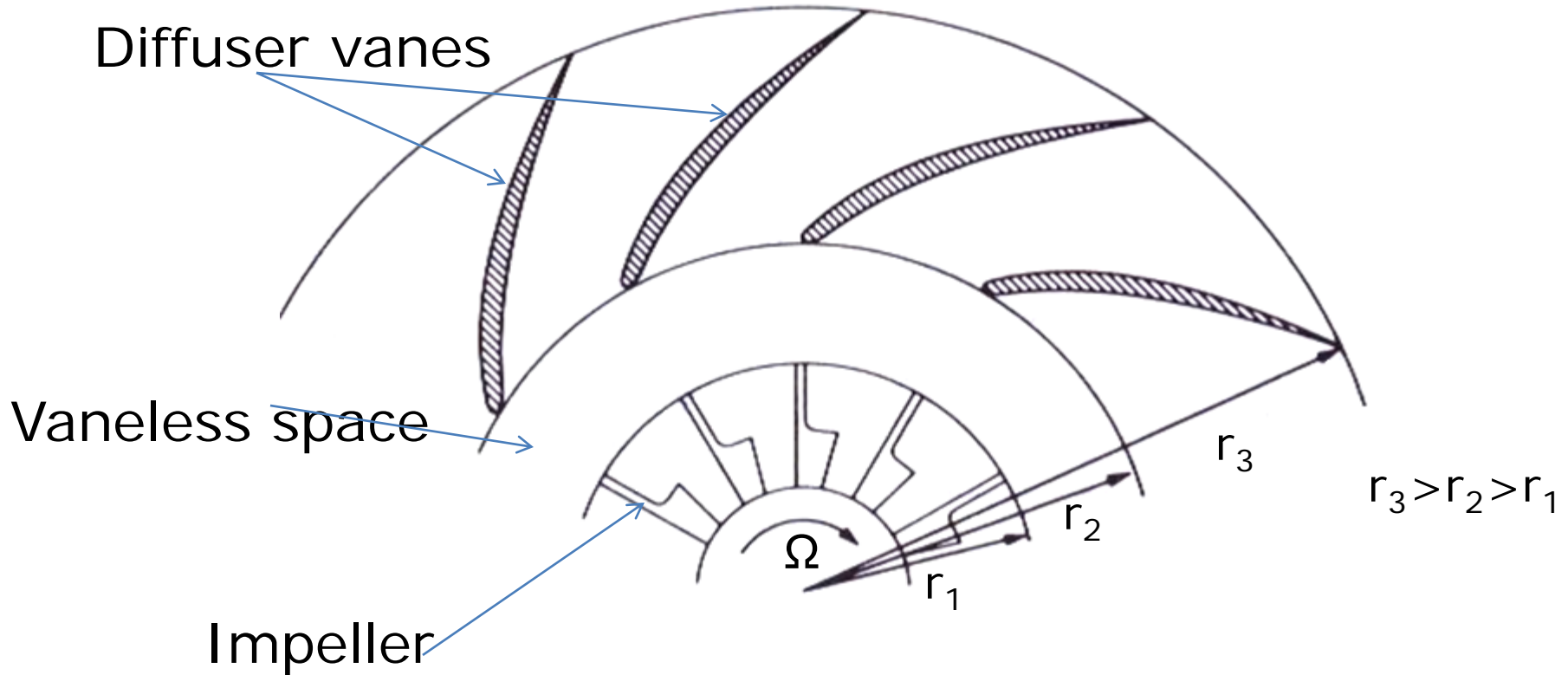
Coriolis acceleration



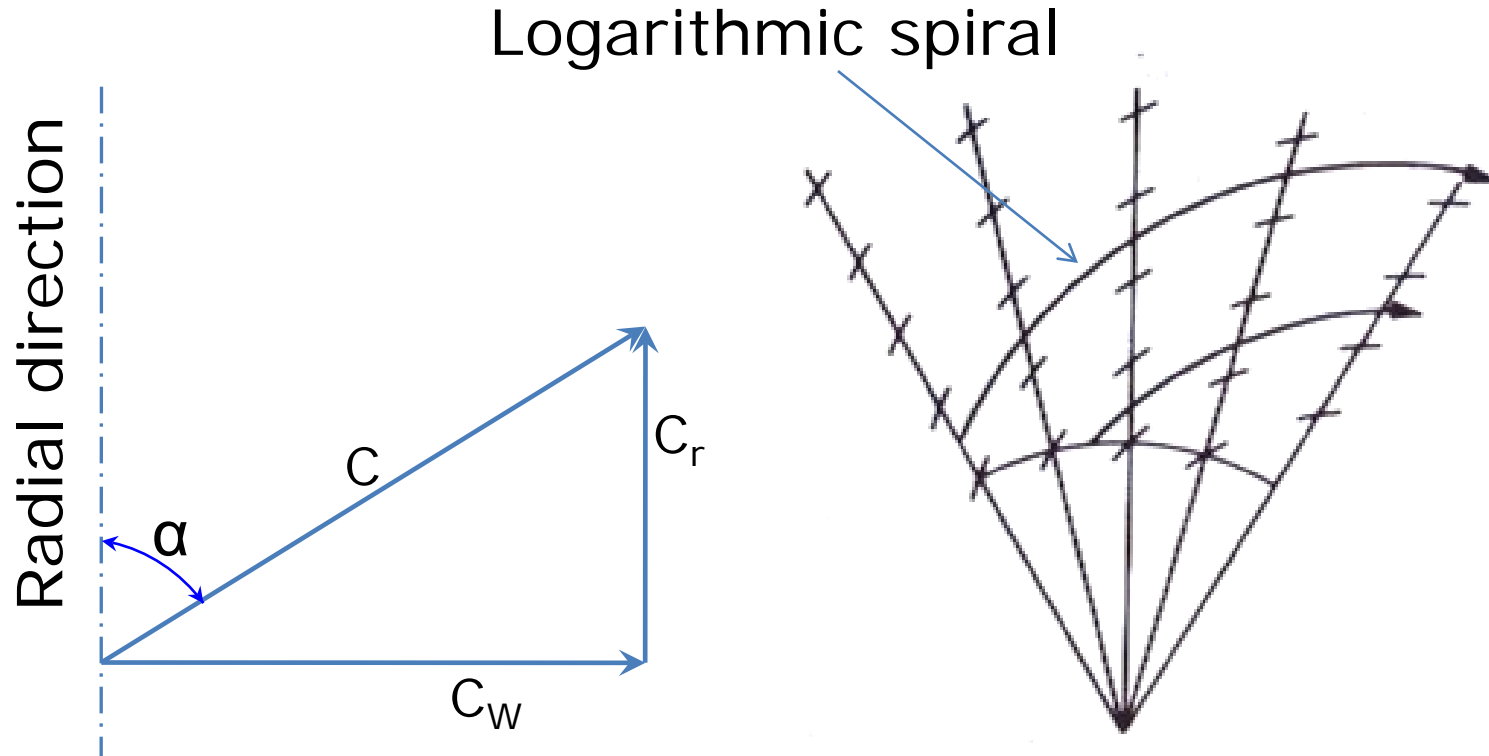
The diffuser

- High impeller speed results in a high absolute Mach number leaving the impeller.
- This high velocity is reduced (with an increase in pressure) in a diffuser.
- The fluid flows radially outwards from the impeller, through a vaneless region and then through a vaned diffuser.
- Both vaned and the vaneless diffusers are controlled by boundary layer behaviour.

The diffuser



The diffuser



Streamlines in a radial diffuser

The diffuser

Let us consider an incompressible flow in a vaneless region of constant axial width.

From continuity, $\dot{m} = \rho(2\pi rh)C_r = \text{constant}$.

From conservation of angular momentum,

$$rC_w = \text{constant}$$

$\therefore C_w/C_r = \text{constant} = \tan \alpha$, where α is the angle between the velocity and the radial direction.

Thus, the velocity is inversely proportional to radius. This means that there is diffusion taking place in the vaneless space.

In this lecture...

- Elements of centrifugal compressors

In the next lecture...

- Performance characteristics of centrifugal compressors
- Surging and choking